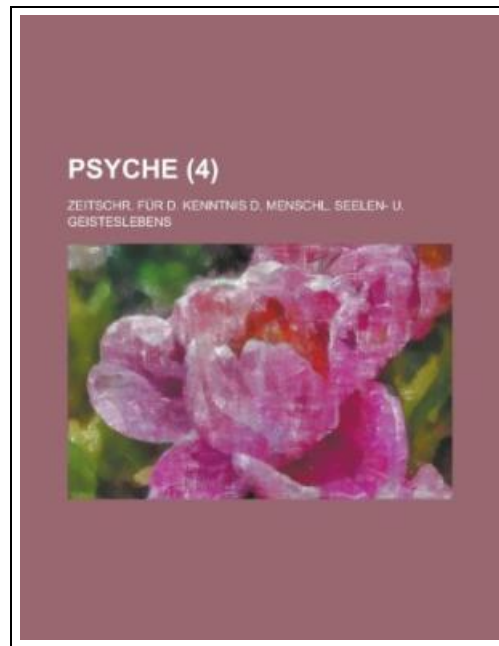


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RareBooksClub. Paperback. Book Condition: New. This item is printed on demand. Paperback. 118 pages. Original publisher: Golden, Colo. : National Renewable Energy Laboratory, 2006 OCLC Number: (OCoLC)177064777 Subject: Biomass energy -- Economic aspects. Excerpt: . . . Section 1 Process Selection Rationale requirements to the selectivity of the amine solvents. Attempts were also made to choose solvents that minimized net energy requirements. Water-Gas Shift and CO Removal 2 FT synthesis requires a H CO ratio of 2: 1, and methanol synthesis requires the following 2 stoichiometric ratio of H, CO, and CO: 2 2 (H - CO) (CO CO) 2 2 2 2 The syngas stream exiting the ZnO beds has a H CO ratio of 1. 7 and a stoichiometric ratio of 2 0. 89, which are inadequate for FT or methanol synthesis. A combination of water injection into the tar cracker, followed by CO removal in the amine unit, has been selected to adjust these 2 ratios. In methanol synthesis, H will react preferentially with CO over CO to form methanol. 2 2 This results in a significantly lowered methanol yield, greatly impacting the process efficiency. In FT synthesis, CO acts as a diluent; however, for a design in which the off-gas from the FT 2 reactor is recycled back to the reactor to improve conversion, removal of CO is necessary to 2 prevent CO buildup in the reactor. 2 The initial designs for the low pressure system incorporated a shift reactor instead of water injection to assist in obtaining the necessary composition ratios. Further analysis and review with NREL led to the determination that a shift reactor was unnecessary, and that steam injection into the tar cracker is sufficient to perform the required shift. Elimination of this unit operation helps to reduce the...



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